

Flocculation Performance and Shearing Capacity Study on Al₃₀ Morphology in Polyhydroxy Aluminium

S.J. JIANG, X.R. FENG^{*}, X.E. LI, P. XIANG and G.S. SHENG

Key laboratory of the Three Gorges Reservoir Region's Eco-environments, Ministry of Education, Chongqing University, Chongqing 400045, P.R. China

*Corresponding author: Tel/Fax: +86 23 65120759; E-mail: fxrgreat@163.com

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As a newly discovered polyaluminum morphology after Al_{13} , Al_{30} is the highest charge cation of polyhydroxy aluminum so far. By comparative analyzing synthetic Al_{30} , Al_{13} and commercial polyaluminum chloride, test results show that Al_{30} has optimal coagulation effect by contrasting turbidity, UV_{254} removal efficiencies and electric neutralization capacity. The particle size analysis of flocculated kaolin micro particles shows that the three flocculants can combine with kaolin particles below 10 µm. The floc size in Al_{30} is the largest, followed by Al_{13} and then polyaluminum chloride, which further proved the advantage of Al_{30} in flocculation process. The conventional jar test and the monitoring technique of floc size online are employed to investigate the shearing capacity of the flocs formed by Al_{30} . It is found that remixing can make the broken flocs fully recovered and the particle size of recovered flocs are greatly increased, especially in Al_{30} .

Key Words: Polyaluminum chloride, Flocculation performance, Particle size analysis, Breakage, Recovery.

INTRODUCTION

Polyaluminum chloride (PAC) is a main stream flocculant in water and wastewater treatment industry. It has characteristics of low dosage, strong charge neutralization capacity¹, forming dense flocs², producing less sludge³, *etc.*, which are closely related to the highly charged polyhydroxy aluminum cation in polyaluminum chloride. For a long time, researchers believed that $[AIO_4AI1_2(OH)_{24}(H_2O)_{12}]^{7+}$ (abbreviated as AI_{13}) as the representative aggregation form plays a critical role in flocculation performance. Studies on the generation, morphological identification⁴ and flocculation performance⁵ of AI_{13} are numerous and long-lasting.

In recent years, with the improvement of analysis technologies, a new polyaluminum morphology larger than Al_{13} was found. This was Al_{30} . In 2000, based on the study of AlP_1 , AlP_2 and AlP_3 , Rowsell and Nazar⁶ proposed that the structure of AlP_2 was Al_{30} ($[Al_{30}O_8(OH)_{56}(H_2O)_{24}]^{18+}$). In the same year, Allouche *et al.*⁷ also proposed the same structure of Al_{30} . The structure consists of two δ - Al_{13} through four hexacoordinated aluminum octahedral coupled together, with 18 positive electric charges. Al_{30} is the new largest polyhydroxy aluminum cation so far. Study on the flocculation performance and mechanism of Al_{30} is important to the development of its series efficient flocculants.

Generally speaking, coagulation process consists of two phases: rapid mixing stage after coagulant dosage and slow flocculation stage that flocs gradually shaped. Since to velocity gradient is maldistributed in coagulation structures, flocs fractured easily and broken flocs can also occur flocculation. In addition, in some stirring intensity, the breakage and recovery processes are concurrence, eventually reaching to a stable dynamic balance. After flocs are broken, if an appropriate slow stirring velocity is imposed, there will be varying degrees of recovery. Researches on aluminum sulfate salts as flocculant had shown that recovery degree of flocs is related to coagulation mechanism. The flocs in charge neutralization flocculation can be fully recovered, however in sweep flocculation process, the flocs are difficult to recover⁸.

Now, researches on floc breakage and recovery situation are mainly for single-molecule traditional flocculants. Polyaluminum chloride as the mainstream flocculant has not been systematically studied. Researches on Al₁₃ and Al₃₀ series flocculants are empty. Such flocculants are different with traditional one-component flocculant in the molecular structure, hydrolysis precipitation, floc morphology and characteristics^{9,10}. For this reason, results from traditional flocculants can not be used into composite macromolecular flocculants. System studies on floc breakage and recovery processes are necessary. This paper used kaolin suspension as simulated wastewater and comparative analyzed floc breakage and recovery capacity of commercial polyaluminum chloride, synthetic Al₁₃ and Al₃₀ through investigating residual turbidity and floc particle size in jar test.

EXPERIMENTAL

The Al₃₀ sample with total Al concentration of 0.2 mol L⁻¹ were prepared by the following method: 20 mL AlC₁₃ aqueous solution with Al concentration of 1.0 mol L⁻¹ was added into 250 mL glass reactor equipped with a Teflon anchor stirrer and a reflux condenser. The solution was heated to a predetermined temperature (80 °C) using a thermostatic apparatus, then 80 mL of aqueous solution of NaOH with a calculated concentration (0.6 mol L^{-1} for B = 2.4) was pumped into the reactor through peristaltic pump at a speed of 0.5 ml min⁻¹ under rapid stirring until the hydrolysis ratio ($B = [OH^{-}]/[Al^{3+}]$) reached a prearranged value. After the addition of NaOH solution finished, the reactants were continuously stirred and heated at a predetermined temperature. This sample was PAC with high content of Al₁₃ (PAC-Al₁₃). PAC-Al₃₀ were prepared by heating PAC-Al₁₃ solution at 95 °C for 36 h. under stirring and refluxing.

Detection method: Coagulation experiments were carried out at room temperature using jar test on a six-paddle gang stirrer (ZR4-6, Zhongrun Co., China). A measured amount of flocculant was added into the water sample under rapid stirring. The characteristics of the water sample are given in Table-1. The water solution was stirred rapidly at 200 rpm for 3 min after coagulant dosing, followed by slow stirring at 50 rpm for 13 min and then settled for 40 min. While in floc breakage and recovery experiment, after slow stirred in normal coagulation procedures above, continue to stir rapidly at 200 rpm for 2 min, followed by slow stirring at 50 rpm for 10 min and then settled for 10 min. Monitor the change of floc particle size online in the entire process and residual turbidity after settlement.

TABLE-1 CHARACTERISTICS OF RAW WATER						
Indexes	Kaolin (mg L ⁻¹)	Humic acid (mg L ⁻¹)	UV ₂₅₄	Turbidity (NTU)	Zeta (mV)	pН
	100	10	0.38	49.6	-25	7.5

The development of floc size during the flocculation period was measured on a Laser Particle Size and Shape Analyzer (Winner 2000, Winner Co., China). The sample was taken using a syringe immediately after coagulant addition and rapid mixing to measure the Zeta potential in Zetasizer Nano ZS90 (Malvern Co., UK). Supernatant sample was withdrawn and filtered through the common qualitative filter paper for UV₂₅₄. UV₂₅₄ representing humic acid concentration was measured at 254 nm through a DR5000 UV spectrophotometer (HACH Co., USA). After settlement, take the sample to measure residual turbidity in a 2100P turbidimeter (HACH Co., USA) and pH through a PHs-3c (Dapu Co., China).

RESULTS AND DISCUSSION

The mechanisms to explain the coagulation of humic substances include charge neutralization, precipitation, bridgeaggregation, adsorption and sweep-flocculation^{11,12}. Under different conditions, the different mechanisms or their combination may be dominant. Because of the high positive charge and big molecular Al₃₀, charge neutralization and bridgeaggregation may play a more important role.

Distribution of Al species: The prepared samples were analyzed by ²⁷Al nuclear magnetic resonance technology. Al₁₃ species are 80.3 % in unmatured product¹³, while Al₃₀ species are 76.8 % in aging product¹⁴. So we called the unmatured product Al₁₃ and aging product Al₃₀. Al_a, Al_b and Al_c were measured in commercial PAC, Al₁₃ and Al₃₀ through Al-Ferron timed complex colorimetric method¹⁵. In commercial PAC, the proportion of Al_a, Al_b and Al_c are 23.97, 64.78 and 11.25 %, while in Al₁₃, Alb is the main form, taking over 88.4 %. In synthetic Al₃₀, Al_c is 73.6 % and Al_b takes 24.3 %. So aluminum monomer is precious little in Al₃₀.

Comparison of charge neutralization capacity: Coagulation experiments were carried out using synthetic PAC-Al₁₃, PAC-Al₃₀ and commercial PAC. As shown in Fig. 1, the dosages of PAC, Al₁₃ and Al₃₀ are 8, 6.8 and 5.72 mg/L respectively when they reach to zero electric potential point. The charge neutralization capacity of Al₃₀ performs complexly. When in low dosage, the charge neutralization capacity is lower than Al₁₃. While the system electric potential is close to neutralization (*i.e.*, when the system electric potential is close to -5 to +5 mV), the charge neutralization capacity of Al₃₀ is stronger than Al₁₃. According to the dosage in zero electric potential point, the order of the three flocculants charge neutralization capacity is Al₃₀ > Al₁₃ > PAC, which is related to Al₃₀ with high charge.

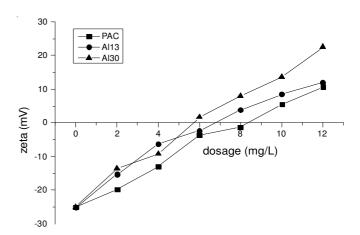


Fig. 1. Comparison of charge neutralization capacity of PAC, Al_{13} and Al_{30}

Comparison of removal efficiency of turbidity: As shown in Fig. 2, turbidity removal efficiency of all the three kinds of flocculants can reach to more than 97 % in kaolin simulated water sample. When the dosage is in 4 mg/L or above, PAC and Al₁₃, RT curves coincide. Residual turbidity curves tend to be gentle after the dosage reaching to 10 mg/L. The removal efficiency of turbidity of Al₃₀ is higher than another two flocculants. When the dosage is close to 8 mg/L, the system reaches to the best turbidity removal, which is essentially coincident with its zero electric potential point. Fig. 2 showed that the main coagulation mechanisms of the three flocculants are charge neutralization.

Change of pH: Addition of flocculants caused the pH reduction of coagulation system as shown in Fig. 3, of which

the reduction amplitude in descending order is PAC, Al_{13} and then Al_{30} . This is because that the PAC contains more Al^{3+} monomers which cause hydrolysis after being added into water. Hydrolysis causes pH reduction of the coagulation system. However, after high-temperature aging, Al_{30} contains Alb and Al_c as its main forms. There is less pH reduction in Al_{30} .

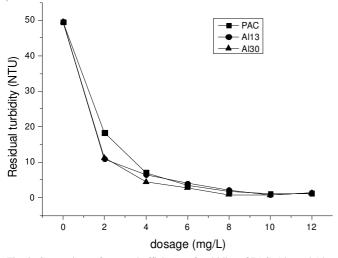


Fig. 2. Comparison of removal efficiency of turbidity of PAC, Al₁₃ and Al₃₀

Comparison of UV₂₅₄ **removal capacity:** UV₂₅₄ has good relation with organic matter in water¹⁶. As shown in Fig. 4, the UV₂₅₄ removal curves of PAC, Al₁₃ and Al₃₀ showed a ladder-type downward trend. When dosages are over 10 mg/L, UV₂₅₄ removal efficiencies of all coagulants can reach to 40 %. According to Fig. 4, UV₂₅₄ removal efficiencies of the three coagulants are not high, because their coagulation mechanisms are mainly charge neutralization rather than adsorption bridging.

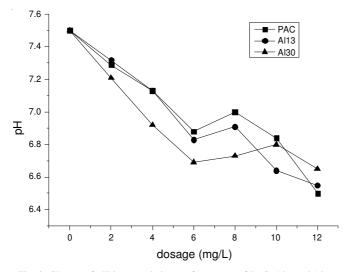


Fig. 3. Change of pH in coagulation performances of PAC, Al_{13} and Al_{30}

Analysis of kaolin microparticle flocculation characteristics: As shown in Fig. 5, three kinds of flocculants have good flocculation abilities on the kaolin simulated water sample with average particle size of 4.08 μ m. Distribution of kaolin particles less than 10 μ m is 0 after flocculation. Viewing from the floc particle sizes, PAC forms floc size between 10 μ m and 30 μ m, while Al₁₃ forms particle size between 40 μ m and 50 μ m. The size of floc formed in Al₃₀ is bigger, more in 50 μ m and 80 μ m. This is because that due to charge neutralization and double electric layers compression, diffusion layers of particles are compressed to reduce the zeta electric potential and to form larger particles under the action of van der Waals force. Al₃₀ has higher electric charge, higher relative molecular mass and stronger charge neutralization capacity than another two flocculants, therefore, the size of floc formed in Al₃₀ is bigger.

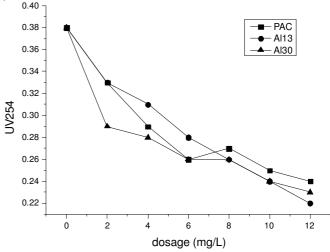


Fig. 4. Comparison of UV254 removal efficiency of PAC, Al13 and Al30

Change of floc size and residual turbidity in floc breakage and recovery process: Floc particle size can directly reflect the floc breakage and recovery condition after remixing. Yukselen and Gregory¹⁷ believed that the grown of flocs is mainly a physical process in charge neutralization flocculation, unrelated to the destruction of chemical bond, as a result, the broken flocs can recover. While in sweep flocculation, the grown of flocs is mainly a chemical process, the broken flocs can lead to destruction of chemical bonds, as a result, the broken flocs are difficult to recover. Some researchers^{14,18,19} have suggested breakage factor (B_f) (Eq. 1) and recovery factor (R_f) (Eq. 2) represent floc broken and recovery degree respectively and strength factor (S_f) (Eq. 3) represents the floc strength.

$$B_{f} = \frac{d_{a} - d_{b}}{d_{a}} \times 100\%$$
(1)

$$R_{f} = \frac{d_{c} - d_{b}}{d_{a} - d_{b}} \times 100\%$$
(2)

$$S_{f} = \frac{d_{b}}{d_{a}} \times 100\% \tag{3}$$

In these equations, d_a represents the floc size before broken; d_b represents the minimum particle size after broken, while d_c represents the floc size after recovery.

As shown in Fig. 6, for the same dosage (6 mg/L) in PAC, Al₁₃ and Al₃₀ flocculation processes, remixing leads to floc broken, and hence, floc particle size declines. In the slow stirred process, floc particle sizes of the three flocculants get fully recovery and the recovered particle sizes are bigger than that before broken. In this condition, the B_f of PAC, Al₁₃ and Al₃₀ are 49.3, 34.3 and 31.1 %, respectively. The R_f are 112.4, 159 and 155 % respectively, while the S_f are 68.7, 58.9 and 81.7 %, respectively. Relatively speaking, flocs of Al_{30} are stronger than another two flocculants and more difficult to be broken, processing strong recovery function.

Final residual turbidity after settlement in the system showed different floc breakage and recovery degrees. This experiment investigated remixing influence on residual turbidity and compared with the situation of that was not remixed. Experimental result shows that for the same dosage (6 mg/L), residual turbidity of PAC, Al₁₃ and Al₃₀ are 3.6 NTU, 4.05 NTU and 2.77 NTU when the system was not remixed.

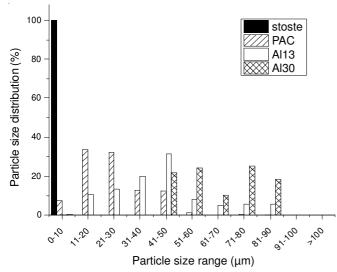


Fig. 5. Kaolin particle size analysis of PAC, Al₁₃ and Al₃₀

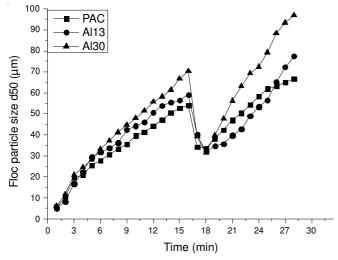


Fig. 6. Change of particle size in floc breakage and recovery process in PAC, Al_{13} and Al_{30}

However, when the system was remixed at 200 rpm, residual turbidity of PAC, Al_{13} and Al_{30} are 3.23 NTU, 2.79 NTU and 2.02 NTU respectively. In all the three coagulation systems, broken flocs after remixing can be fully recovered in charge neutralization flocculation zone and residual turbidity

of the systems are significantly lower after remixing. This experiment further proves the stability of Al₃₀ in flocculation process.

Conclusion

By contrasting turbidity and UV₂₅₄ removal efficiencies, charge neutralization capacity and change of pH in commercial PAC, synthetic Al₁₃ and Al₃₀, analysis result showed that charge neutralization is the main mechanism of the three flocculants, ofwhich the charge neutralization capacity in Al₃₀ is better than another two flocculants with minimum pH variation. Flocculation effect of Al₃₀ is the best flocculants. By contrasting particle size of kaolin flocculation microparticles in commercial PAC, synthetic Al₁₃ and Al₃₀, the three flocculants can be combined with kaolin particles less than 10 µm. The order of floc particle size is Al₃₀ > Al₁₃ > PAC, which further demonstrates the superiority of Al₃₀ in flocculation process.

In floc breakage and recovery experiment, remixing can make the broken flocs fully recovered and the particle size of recovered flocs are greatly increased. At the same time, residual turbidity has also been reduced. All of this further proves the stability of Al_{30} in flocculation process.

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