



Adsorption Studies of Removal of Indigo Carmine Dye from Water by Formaldehyde and Urea Treated Cellulosic Waste of *Citrus reticulata* Peels

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The *Citrus reticulata* (orange) peels has been employed as adsorbents for removing inorganic and organic pollutants from wastewater extensively due to its low cost and eco-friendly nature. This research work concerns with the study of comparative removal of Indigo carmine dye from water using simple, formaldehyde and urea treated *Citrus reticulata* peels. The effect of adsorption parameters were investigated and maximum sorption capacity was obtained from Langmuir isotherm model at optimized conditions, *i.e.*: 5.90, 14.79 and 71.07 mg g⁻¹ for simple, formaldehyde treated and urea treated *Citrus reticulata* peels, respectively. Feasibility of process is indicated by the values of separation factor, Gibb's free energy and adsorption intensity 'n'. The results of present study indicate that *Citrus reticulata* peels has inherited a lots of capacity for removing anthraquinone type of dyes, which can be further improved by treating with formaldehyde or urea in economical way.

Keywords: *Citrus reticulata* peels, Indigo carmine dye, Chemical modification, Isothermal study.

INTRODUCTION

Development of industries have large impact on environment. Many industries used dyes which contains much organic and inorganic colour causing compound. Fraction of dye lost in wastewater during dye-processing is 50 % of dye used, due to their low fiber fixation value^{1,2}. Even 1 ppm of dye in water make it non-suitable for human use³. Dye can also disturb marine life and plants because they reduced the sunlight penetration in water. They are carcinogenic and cause a detrimental effect on human beings, such as liver, brain, central nervous system, reproductive system *etc.*⁴⁻⁶. The removal of dye from water is necessary because its small amount is very toxic and dangerous⁷. Many technique have been used to eradicate these pollutant from wastewater, like photochemical oxidation, coagulation, membrane filtration, electro-chemical and bacteriological degradation, *etc.*⁸. Wastewater released from textile contain organic compound, heavy metal, total dissolve solid, PCBs, surfactant, COD, BOD, salts^{9,10}.

Dyes are usually categorized into cationic, anionic and non-ionic. Generally cationic dyes are basic in nature, whereas anionic dyes are acidic. Anionic dyes depend on the negatively charge ion¹¹. They contain many compound, which have characteristic difference in structures (like: anthraquinone, triphenyl-methane, azoic and nitro dyes). Anthraquinonic types are more lethal, because of non-degradable nature¹². They are

used to dye synthetic fibers like modified acrylic, silk, polyamide and polypropylene. Their water soluble tendency is greater, but have a destructive effect on living things, because they have organic sulphonic acid group¹³.

The adsorption of anionic dyes using different adsorbents have studied by many researchers using bentonite, ammonium functionalized MCM 41, plant leaves, seeds, pine cone and bagasse ash¹⁴⁻¹⁷. The agricultural waste used in last few years has been low cost and the available adsorbent used for sorption of anionic/acidic dyes such as mango seeds, soymeal, rice/wheat husk and bamboo^{11,12,18}.

In this research work, *Citrus reticulata* peels was used to remove Indigo carmine dye. This dye is a pH indicator, structure is given in Fig. 1. At pH 11.4, it exists in blue colour while at 13, it exists in yellow colour. It is also a redox indicator, on reduction it turns into yellow colour. It is used as food colourant in USA. It is also used as a dye in the formation of capsules, obstetrics and help to detect amniotic fluid leaks. If it is inhaled it is harmful to the respiratory tract and causes skin and eye irritations¹⁹⁻²¹. *Citrus reticulata* (common known as Kinnow or orange) belongs to plant family Rutaceae, usually reach a height of 25 feet on average with a greater spread. Pakistan is the one of the leading producer in the world and produces almost 95 % of the total Kinnow production of the world. In traditional Ayurvedic herbal medicines, the dried peels of *Citrus reticulata* fruit is used to treat abdominal distension and reduce phlegm by enhancing digestion²²⁻²⁴.

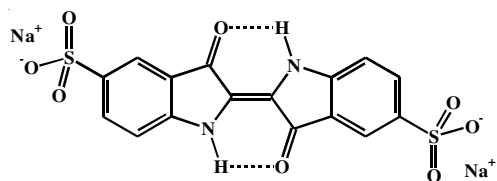


Fig. 1. Indigo Carmine (IUPAC name: 3,3'-dioxo-2,2'-bis-indolyden-5,5'-disulfonic acid disodium)

EXPERIMENTAL

Indigo carmine [chemical formula $C_{16}H_8N_2O_8S_2Na_2$, m.w. = 466.36 g/mol, $\lambda_{max} = 610$ nm], HCl, NaOH, urea and formaldehyde used in this research work (obtained from Fluka and Riedel-de Haen). pH meter (HANNA pH 211), spectrophotometer (Spectro UVD-3500, Labomed), Scanning Electron Microscope (SEM) S2700 Hitachi, Japan and FT-IR spectrometer (Perkin Elmer, ATR) were used for analysis. Dye stock solution was synthesized by dissolving its 1 g/L of water (double distilled) and afterward diluted according to experimental needs.

Preparation of biosorbents: Fresh oranges (*Citrus reticulata*) were collected from local gardens of Lahore (Pakistan) and washed. Their peels were removed and dried in sunlight for a week. Then they were placed in oven at 70 °C for 4 h. For chemical treatment, 100 g chopped, dried peels were soaked in 500 mL of 20 % formaldehyde and 10 % urea solutions separately for 3 h. Then they were filtered and dried in air after covering with cloth to prevent contaminations for 3 days. For complete removal of moisture, they were kept in oven at 70 °C for 4 h. All these dried samples of simple (S.B), formaldehyde treated (F.T.B) and urea treated (U.T.B) *Citrus reticulata* peels were ground using electric grinder (Ken-Wood) and sieved through 50 mesh ASTM (297 microns). They were stored in plastic jars separately.

Adsorption studies: Following factors were studied in their respective ranges as followed in batch mode one after another, keeping one factor variable at a time and others constant: contact time interval (10-70 min), dye solution pH (1-10), adsorbent dosage (0.3-3.0 g) and temperature (20-70 °C). Constant mixing of the solution was provided by a agitating at 100 rpm. After adsorption, the adsorbent was separated from the solution and remaining concentration of dye was determined spectrometrically at $\lambda_{max} = 610$ nm. The percentage adsorption of dye was determined by eqn. 1²⁵:

$$\text{Removal (\%)} \text{ of dye} = \frac{C_o - C_e}{C_o} \times 100 \quad (1)$$

The volume (V) of dye solution used in various steps was 0.05 L and initial concentration of dye 'C_o' was 25 mg/L. For determining mechanism of removal of dye and feasibility of process, isothermal modeling of equilibrium data was done. Batchwise adsorption of dye was performed by using all the optimized conditions of various parameters on dye solutions with concentration ranges 30-80 mg/L. Then after quantifying remaining concentration of dye "C_e" adsorption capacities 'q' was calculated by eqn. 2:

$$q = \frac{(C_o - C_e)V}{m} \quad (2)$$

Langmuir and Freundlich models were applied on equilibrium data using their straight line eqns. 3 and 4, respectively:

$$\log q = \log K_F + \frac{1}{n} \log C_e \quad (3)$$

$$\frac{1}{q} = \frac{1}{bq_m C_e} + \frac{1}{q_m} \quad (4)$$

here, 'q_m' and 'b' are Langmuir parameters, whereas 'K_F' and 'n' are Freundlich parameters. Their values were determined by regression analysis of linear plots of respective isotherms. Experiments were repeated thrice and average values were used for calculations. Basic assumption of Langmuir model is that chemisorption of adsorbate occurs in monolayer fashion on adsorbent surface in homogenous way and there are no side interactions between adsorbed species molecules, whereas Freundlich model assumes multilayer physisorption of adsorbate species on heterogeneously distributed binding sites on adsorbent surface. Feasibility of process is determined by separation factor, 'R_L' and Gibb's free energy 'ΔG°', which are determined by eqns. 5 and 6, respectively:

$$R_L = \frac{1}{(1 + bC_o)} \quad (5)$$

$$\Delta G^\circ = -RT \ln K \quad (6)$$

here, 'K' is the reciprocal of Langmuir constant 'b'. R_L value less than zero indicate unfavorable process, whereas in between zero to unity indicate favorable process^{26,27}.

RESULTS AND DISCUSSION

Characterization of biosorbents: *Citrus reticulata* peels mostly consists of cellulosic material having reactive hydrogen atom. Formaldehyde undergoes addition reaction with compounds containing reactive hydrogen atom to form methylol derivatives (Fig. 2). Whereas hydroxyl groups of carboxylic acids or alcohols present in *Citrus reticulata* peels interact with urea forming condensation product as shown in Fig. 3. These mechanisms were also supported by FT-IR analysis as summarized in Table-1. FT-IR spectrum of *Citrus reticulata* peels indicated the presence of O-H groups by broad peak at 3416 cm⁻¹. In F.T.B, this peak is shifted to 3429 cm⁻¹ supporting the possibility of chemical mechanism (Fig. 2). While this peak is vanished and a new peak at 3791 cm⁻¹ is appeared in U.T.B, supporting second mechanism shown in Fig. 3. Other functional groups peaks values indicated the occurrence of carbonyl, ether and ester groups, that can interact better with acidic dye after protonation in acidic pH range. Further surface analysis were done by taking micrographs with scanning electron micro-

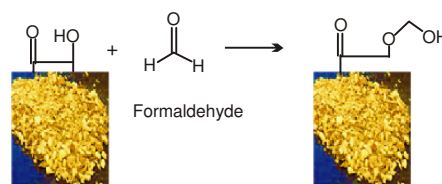
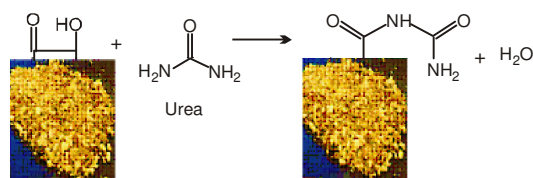


Fig. 2. Possible mechanism of formaldehyde treatment on *Citrus reticulata* peels



Citrus reticulata peels Urea modified *Citrus reticulata* peels

Fig. 3. Possible mechanism of urea treatment on *Citrus reticulata* peels

scope as given in Fig. 4. It is evident from Fig. 4 that after chemical modification with formaldehyde/urea, *Citrus reticulata* peels surface become more rough, uneven with visible pores and canals of irregular shapes permeating into the inner particle structure. These pores were produced after chemical modification, which in turns help in physisorptive removal of Indigo carmine dye²⁰⁻²⁴.

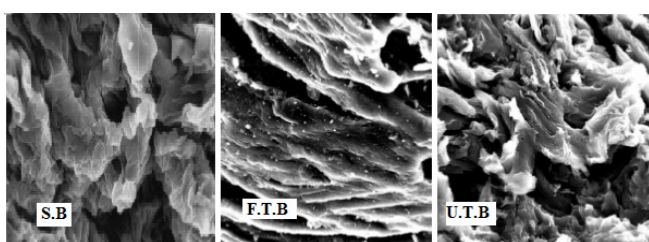


Fig. 4. SEM images of simple and chemically treated *Citrus reticulata* peels

Adsorption parameters

Contact time: Its effect on adsorption of Indigo carmine from aqueous solution by simple and chemically treated biosorbents was studied and the results were shown in Fig. 5. From this figure, it was found that the adsorptive quantity of the dye on all the types of adsorbent almost remained constant and equilibrium was nearly reached after 1 h. The adsorption efficiency, however, was maximum for every point in case of U.T.B. This delayed adsorption trend suggests that physisorption is operative in adsorbing dye ions on biomass, because chemisorption occurred relatively faster than physisorption. Physisorption is generally dominant at low temperature and characterized by a relatively little energy of adsorption²⁸. Hence, in the present experiment, 1 h was chosen as the equilibrium time.

Adsorbate pH: The pH is an important parameter affecting the rate and extent of adsorption. Variation of pH may alter the solubility of ions and surface charge of biosorbent. The effect of pH on adsorption of Indigo carmine dye by *Citrus reticulata* peels is given in Fig. 6. The maximum dye sorption occurred at pH 1-2 in all cases and decreased

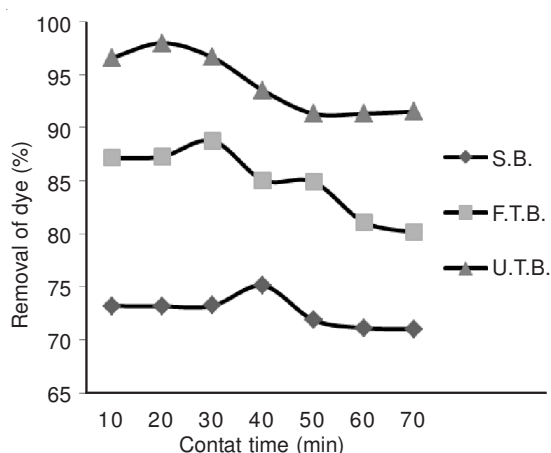


Fig. 5. Effect of contact time on adsorption of Indigo carmine by *Citrus reticulata* peels

thereafter. Acidic dyes are more ionized in lower pH range, which results in larger concentration of ionized species in aquatic medium that can interact more with active binding sites of biosorbent. Indigo carmine is an acidic/anionic dye. In basic conditions, the number of negatively charged active sites on biosorbent surfaces increases, which hindered in adsorption of anionic dye because of electrostatic repulsion. Usually acidic dyes adsorption is much higher in acidic solutions rather than those in high pH conditions^{28,29}.

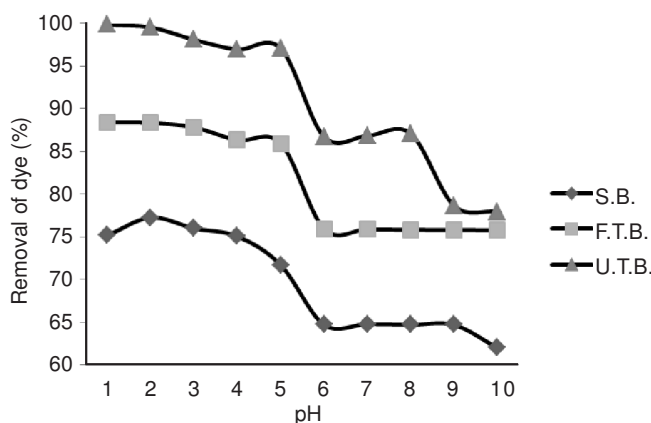


Fig. 6. Effect of pH on adsorption of Indigo carmine by *Citrus reticulata* peels

Adsorbent dosage: The experiment on the influence of adsorbent dosage on adsorption of the dye was done with different dosages. The graph is shown in Fig. 7. Maximum adsorption occurred when adsorbent dose is 1.5, 0.6 and 0.6 g using S.B, F.T.B and U.T.B, respectively. But urea treated biosorbent

TABLE-1
FT-IR SPECTRAL ANALYSIS OF SIMPLE (S.B), FORMALDEHYDE TREATED (F.T.B) AND UREA TREATED (U.T.B) *Citrus reticulata* PEELS

Functional groups vibrational assignments	S.B (cm ⁻¹)	F.T.B (cm ⁻¹)	U.T.B (cm ⁻¹)
N-H stretching (amido, amino groups)	–	–	3791.2
OH stretching (hydroxyl, carboxyl group)	3416	3429	–
C-H stretching (methyl, methylene group in lignin)	2921.01	2918	2629.8
C=O and C=C stretching (carbonyl of aldehyde/ketone)	1639	1627	1695.0
C-H bending	1434.7	1371	1459.3, 1375.5
C-O-C stretching (ether group in carbohydrates)	1049	1055.7	1057.1
O=C-N bending	–	–	548.4

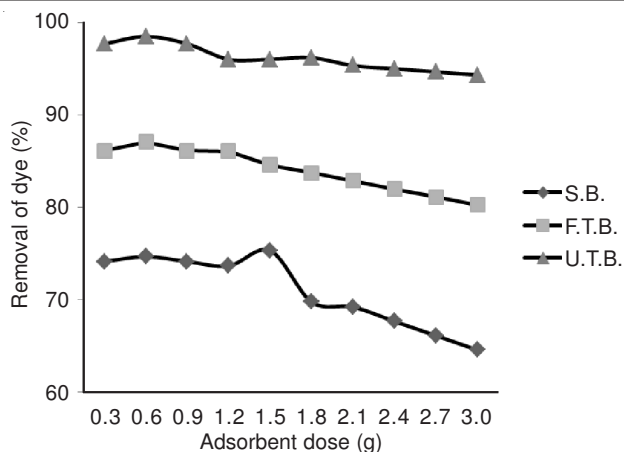


Fig. 7. Effect of adsorbent dose on adsorption of Indigo carmine by *Citrus reticulata* peels

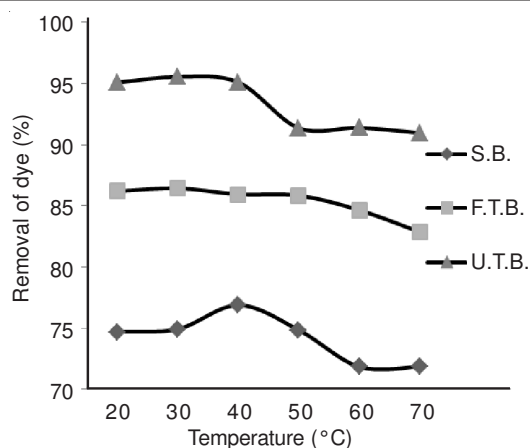


Fig. 8. Effect of temperature on adsorption of Indigo carmine by *Citrus reticulata* peels

adsorb more as compared to simple and formaldehyde treated biosorbents. Amount of available adsorption sites increased with a rise in adsorbent dosage and resulted in better adsorption. After optimized value, decrease in adsorption capacity may be due to the decline in solute transfer rate on biosorbent surface. In literature, a decrease was found in the adsorption efficiency by many researchers, when the adsorbent dose was increased. They suggested that a limited cell accumulation taking place at high adsorbent dose caused reduction of active sites. Various explanations including pH, ionic strength, temperature and dye ions in solution had been suggested to elucidate the reduced adsorption capacity at increasing biomass^{16,22}.

Temperature: Its effect on the adsorption of dyes is very important on large scale application of adsorption as various effluents are produced at quite high temperatures. The adsorption of Indigo carmine dye was investigated as a function of temperature and graphically represented in Fig. 8. Maximum adsorption was obtained at nearly 30 °C in case of S.B, while F.T.B showed maximum value at 60 °C, suggesting that adsorption between the dye and F.T.B was an endothermic process. Adsorption efficiency nearly remained constant in case of U.T.B. The negligible decrease with further increase in temperature in case of S.B and U.T.B due to the decreased surface activity suggesting that adsorption in this case became an exothermic process. In that case, the mechanism was mainly physisorption. It was further confirmed from isothermal investigations²⁶.

Determination of mechanism of adsorption and feasibility of process:

Table-2 shows the Langmuir isothermal parameters while Table-3 shows the Freundlich isothermal parameters for Indigo carmine dye adsorption by *Citrus reticulata* peels. Correlation coefficient values comparison indicated that Freundlich model is applicable more to adsorption data using simple (S.B) and formaldehyde treated biosorbents (F.T.B), while Langmuir model is followed using urea treated biosorbent (U.T.B). It means physio-sorption is the main mode of adsorptive removal of Indigo carmine dye by *Citrus reticulata* peels, when S.B and F.T.B were used, while chemisorption occurred more using U.T.B. Langmuir maximum adsorption capacity parameter ' q_m ' values are: 5.90, 14.79 and 71.07 mg g⁻¹ for S.B, F.T.B and U.T.B, respectively. These values indicated that urea treatment is more effective for chemical treatment, as compared to formaldehyde treatment. This is also evident from previous Figs. 4-7. Freundlich physiosorption constant ' K_F ' values are: 35.27, 77.90 and 26.41 mg^{1-1/n} L^{1/n} g⁻¹ for S.B, F.T.B and U.T.B, respectively. They indicated that formaldehyde treatment is more effective for physiosorptive removal of dye, because formaldehyde dissolves colouring matter and resinous material of *Citrus reticulata* peels, which results in exposure of more binding sites.

Langmuir parameter ' b ' is used to determine separation factor ' R_L ' and thermodynamic parameter ' ΔG° '. Feasibility of using *Citrus reticulata* peels for adsorption of Indigo carmine

TABLE-2
LANGMUIR ISOTHERMAL AND THERMODYNAMICAL PARAMETERS FOR ADSORPTIVE REMOVAL OF INDIGO CARMINE DYE BY CHEMICALLY MODIFIED *Citrus reticulata* PEELS

Biosorbent	Langmuir isotherm parameters					Separation factor R_L	Thermodynamic parameter ΔG° (KJ mol ⁻¹)
	Slope	Intercept	R^2	q_{max} (mg g ⁻¹)	b (L g ⁻¹)		
S.B	0.153	-0.169	0.758	5.90	1.108	0.018	0.254
F.T.B	0.052	-0.068	0.714	14.79	1.289	0.016	0.629
U.T.B	0.045	-0.014	0.875	71.07	0.312	0.069	-2.886

TABLE-3
FREUNDLICH PARAMETERS FOR ADSORPTIVE REMOVAL OF INDIGO CARMINE DYE BY CHEMICALLY MODIFIED *Citrus reticulata* PEELS

Biosorbent	Freundlich isotherm parameters				
	Slope	Intercept	R^2	K_F (mg ^{1-1/n} L ^{1/n} g ⁻¹)	n
S.B	2.223	1.547	0.834	35.27	0.450
F.T.B	1.745	1.892	0.698	77.90	0.573
U.T.B	1.019	1.422	0.861	26.41	0.981

dye were confirmed by separation factor values, 'R_L', which are in between zero to unity, i.e.: 0.018, 0.016 and 0.069 for S.B, F.T.B and U.T.B, respectively. Negative value of Gibb's free energy (ΔG°) indicated that urea treated *Citrus reticulata* peels are more suitable for adsorption of Indigo carmine dye from water. Freundlich constant 'n' values smaller than eight, indicated the practicability of this process at minor concentration of dye²⁶⁻²⁹.

Conclusion

The application of indigenous waste materials from agricultural residues as economical substitution to commercial adsorbents has been demonstrated in this study. This research work indicated that *Citrus reticulata* peels can be effectively used for adsorptive removal of Indigo carmine dye from water. Their adsorption capacity is further enhanced by treating them with formaldehyde and urea separately. Results shown that urea treatment of *Citrus reticulata* peels was more effective for removing anionic dyes from water. Maximum removal of dye by simple, formaldehyde treated and urea treated *Citrus reticulata* peels were: 5.90, 14.79 and 71.07 mg g⁻¹, respectively. So, it is concluded that urea treated *Citrus reticulata* peels can be used on industrial scale for removal of Indigo carmine dye.

REFERENCES

- N. Mohan, N. Balasubramanian and C.A. Basha, *J. Hazard. Mater.*, **147**, 644 (2007).
- M.K. Sharma and R.C. Sobti, *Mutat. Res.-Genetic Toxicol. Environ. Mutagen.*, **465**, 27 (2000).
- R. Malik, D.S. Ramteke and S.R. Wate, *Waste Manage.*, **27**, 1129 (2007).
- K. Kadirvelu, M. Kavipriya, C. Karthika, M. Radhika, N. Vennilamani and S. Pattabhi, *Bioresour. Technol.*, **87**, 129 (2003).
- A.R. Dinçer, Y. Günes, N. Karakaya and E. Güne, *Bioresour. Technol.*, **98**, 834 (2007).
- D. Shen, J. Fan, W. Zhou, B. Gao, Q. Yue and Q. Kang, *J. Hazard. Mater.*, **172**, 99 (2009).
- M.S. Chiou, P.-Y. Ho and H.-Y. Li, *Dyes Pigments*, **60**, 69 (2004).
- M.T. Sulak, E. Demirbas and M. Kobya, *Bioresour. Technol.*, **98**, 2590 (2007).
- K.P. Sharma, S. Sharma, S. Sharma, P.K. Singh, S. Kumar, R. Grover and P.K. Sharma, *Chemosphere*, **69**, 48 (2007).
- S. Sen and G.N. Demirel, *Water Res.*, **37**, 1868 (2003).
- N. Modirshahla, A. Hassani, M.A. Behnajady and R. Rahbarfam, *Desalination*, **271**, 187 (2011).
- N. Daneshvar, H. Ashassi-Sorkhabi and A. Tizpar, *Sep. Purif. Technol.*, **31**, 153 (2003).
- H. El-Boujaady, A. El-Rhilassi, M. Bennani-Ziatni, R. El-Hamri, A. Taitai and J.L. Lacout, *Desalination*, **275**, 10 (2011).
- P. Leechart, W. Nakbanpote and P. Thiravetyan, *J. Environ. Manage.*, **90**, 912 (2009).
- M. Valix, W.H. Cheung and G. McKay, *Chemosphere*, **56**, 493 (2004).
- M.M. Dávila-Jiménez, M.P. Elizalde-González and V. Hernández-Montoya, *Bioresour. Technol.*, **100**, 6199 (2009).
- M.A. Behnajady, N. Modirshahla and R. Hamzavi, *J. Hazard. Mater.*, **133**, 226 (2006).
- J.L. Wang and J.Z. Wang, *J. Hazard. Mater.*, **143**, 2 (2007).
- X. Zhang, F. Zhao and K.A. Li, *Microchem. J.*, **68**, 53 (2001).
- Y.R. Sheynkin, C. Starr, P.S. Li and M. Goldstein, *Urology*, **53**, 214 (1999).
- F.V. de Andrade, G.M. de Lima, R. Augusti, M.G. Coelho, J.D. Ardisson and O.B. Romero, *Chem. Eng. J.*, **180**, 25 (2012).
- S. Liang, X. Guo, N. Feng and Q. Tian, *J. Hazard. Mater.*, **170**, 425 (2009).
- P. Velmurugan, V.R. Kumar and G. Dhinakaran, *Int. J. Environ. Sci.*, **1**, 1492 (2011).
- M. Arami, N.Y. Limaee, N.M. Mahmoodi and N.S. Tabrizi, *J. Colloid Interf. Sci.*, **288**, 371 (2005).
- R. Rehman and T. Mahmud, Proceeding of ICENV, Penang, Malaysia, p. 103 (2012).
- F. Kanwal, R. Rehman, J. Anwar and M. Saeed, *Asian J. Chem.*, **25**, 2399 (2013).
- A. Mittal, J. Mittal and L. Kurup, *J. Hazard. Mater.*, **137**, 591 (2006).
- S.M. de Oliveira Brito, H.M.C. Andrade, L.F. Soares and R.P. de Azevedo, *J. Hazard. Mater.*, **174**, 84 (2010).
- U.R. Lakshmi, V.C. Srivastava, I.D. Mall and D.H. Lataye, *J. Environ. Manage.*, **90**, 710 (2009).