

## Adsorption of Divalent Metal Ions on a Herbaceous Peat

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This study was performed to determine divalent metal ion [Cu(II), Zn(II), Mn(II) and Ni(II)] adsorption characteristics of the herbaceous peat of the Gavur Lake, Turkey. The adsorption data of the metal ions were fitted to both the Langmuir and the Freundlich isotherms. The adsorption capacity of the peat was much higher for Cu (38.5 mg g<sup>-1</sup>) compared with Zn (28.0 mg g<sup>-1</sup>), Mn (26.4 mg g<sup>-1</sup>) and Ni (24.1 mg g<sup>-1</sup>). A steady increase in equilibrium Ca and Mg ion concentrations were measured as initial metal ion concentrations increased from 1 × 10<sup>-3</sup> M to 5 × 10<sup>-3</sup> M in Cu and Zn adsorption experiments indicating that ion exchange was an important mechanism in the adsorption. The kinetic study revealed that the adsorption followed the pseudo-second-order model and the interaction between the metal ions and the peat was very fast, especially for Cu. The pH study revealed that Cu adsorption was not affected in the pH range between 3 and 5, but the adsorption of Zn, Mn and Ni was lower at pH 3 compared with pH 4 and 5.

**Key Words:** Adsorption, Kinetics, Peat, Copper, Zinc, Manganese, Nickel.

### INTRODUCTION

There is an increasing environmental concern of heavy metal loading to water resources from industrial wastewater discharges. High levels of the heavy metals such as copper, zinc, manganese and nickel are harmful for many life forms and cause brain, kidney, lungs, liver and central nervous systems failure in humans<sup>1</sup>. Copper is released to environment *via* mining, metallurgical, fibre production, pipe production and metal plating industries. Zinc is mainly used in galvanization processes; nickel is important for electroplating and manganese finds its use in dry cell batteries, glass, ceramics, paint, varnish, ink, dyes, match and fire works<sup>2</sup>.

Many processes exist for the treatment of wastewaters including ion exchange, precipitation, phyto-extraction, ultra-filtration, reverse osmosis and electro-dialysis and among these methods ion exchange seems most promising due to easy handling if effective and low cost sorbents are used<sup>3</sup>. The adsorption of metal ions from aqueous solutions has been studied using more than 70 different sorbents<sup>4</sup> such as perlite<sup>5</sup>, vermiculite<sup>6</sup>, kaolinite<sup>7</sup>, tree fern<sup>8</sup>, palm kernel fibre<sup>9</sup>, carbon aerogel<sup>2</sup>, Nipah palm shoot biomass<sup>10</sup>, clinoptilolite<sup>3</sup>, fly ash<sup>11</sup> and peat<sup>12,13</sup>. Peat has polar functional

groups such as aldehydes, ketones and acids<sup>13</sup>. Metal ion adsorption by peat may take place *via* several mechanisms such as ion-exchange, surface sorption, chemisorption, complexation and sorption-complexation and it is believed that ion-exchange is the most prevalent mechanism<sup>12</sup>. The metal adsorption capacity of peat depends on many factors such as pH, temperature, contact time, peat dose, botanical origin of peat, metal ion and initial metal ion concentration<sup>13,14</sup>. This study was performed to determine Cu(II), Zn(II), Mn(II) and Ni(II) sorption characteristics of the herbaceous peat of the Gavur lake, Turkey.

### EXPERIMENTAL

The herbaceous peat used in this study was obtained from the Gavur lake Peatland of Turkey. The peatland, which is surrounded by Miocene aged limestone and Paleozoic schist and serpentines formed on Holocene aged lake deposits in a closed watershed<sup>15</sup> on the Antakya-Kahramanmaras Graben, *ca.* 475-481 m asl, 30 km south of the Kahramanmaras city, Turkey. The area was drained by the State Hydraulic Works in the late 1950s using artificial canal networks which flow into the Aksu and Ceyhan rivers.

The peat sample was oven dried at 105 °C and grounded through a 100 µm sieve. The soil sample was analyzed for organic matter by wet oxidation<sup>16</sup>, pH<sup>17</sup> and CaCO<sub>3</sub><sup>18</sup>. The studied peat material has 53.6 % organic matter, neutral pH and 4.3 % total carbonate content (Table-1).

TABLE-1  
SOME PHYSICAL CHARACTERISTICS OF THE PEAT MATERIAL

Organic matter (%)	53.6
pH	6.97
Total carbonate (%)	4.30

**Adsorption experiment:** Copper, Zn, Mn and Ni stock solutions were prepared using analytical grade CuSO<sub>4</sub>.5H<sub>2</sub>O, ZnCl<sub>2</sub>, MnCl<sub>2</sub>.4H<sub>2</sub>O and NiCl<sub>2</sub>.6H<sub>2</sub>O. A 0.5 g soil sample was weighed into a 125 mL Erlenmeyer flask and 50 mL solution containing between  $1 \times 10^{-3}$  M and  $5 \times 10^{-3}$  M concentrations of the studied metal ions ( $63.5$ - $317.5$  µg mL<sup>-1</sup> for Cu) were added into each flask. The adsorption experiments were run in triplicates. Initial pH of the solutions was adjusted to 5, except the pH study, using  $1 \times 10^{-3}$  M solutions of either H<sub>2</sub>SO<sub>4</sub> or NaOH. The flasks were shaken for 3 h at  $21 \pm 1$  °C and filtered. Equilibrium metal ion concentrations were determined using an atomic absorption spectrometer (Perkin-Elmer 3110). The amount of metal ion adsorbed by peat was calculated by the difference between the initial and equilibrium concentrations of the solutions.

In order to show the effect of cation exchange in the adsorption process, the displacement of Ca and Mg ions in Cu and Zn experiments was measured using an atomic absorption spectrometer (Perkin-Elmer 3110).

The effect of solution pH on metal ion adsorption was studied in the pH range between 3 and 5. Initial pH of the solutions was adjusted to 3, 4 and 5 using  $1 \times 10^{-3}$  M solutions of either  $H_2SO_4$  or NaOH and the flasks were shaken for 3 h at  $21 \pm 1$  °C and filtered. The concentrations of the metal ions in equilibrium solutions were determined as mentioned above.

Kinetics of the adsorption were studied by shaking a 0.5 g peat sample with 50 mL solutions of  $2 \times 10^{-3}$  M and  $4 \times 10^{-3}$  M metal ions in a 125 mL Erlenmeyer flask. Samples were withdrawn at suitable time intervals up to 3 h, filtered and analyzed for the studied metals with an atomic absorption spectrometer (Perkin-Elmer 3110).

**Theoretical:** The metal adsorption by the peat was modeled using the Langmuir and Freundlich isotherms. The Langmuir model implies that the monolayer adsorption of metal ions on sorbent surface occurs, energy of sorption for each ion is same and not dependent on surface coverage and adsorption takes place only on localized sites<sup>13</sup>. The Freundlich model, however, assumes that the energy of adsorption decreases logarithmically as surface coverage increases due to surface heterogeneity.

#### Langmuir isotherm:

$$C_e/q_e = 1/kq_{\max} + C_e/q_{\max}$$

where  $q_e$  is the amount of adsorbed metal ion by the peat ( $mg\ g^{-1}$ ),  $C_e$  is the equilibrium solution concentrations ( $mg\ L^{-1}$ ),  $q_{\max}$  is the adsorption maximum or the adsorption capacity ( $mg\ g^{-1}$ ) and  $k$  is a constant related to the sorption energy ( $L\ mg^{-1}$ ). If adsorption conforms to the Langmuir equation, a plot of  $C_e/q_e$  vs.  $C_e$  will form a straight line with a slope  $1/q_{\max}$  and intercept  $1/k \times q_{\max}$ .

#### Freundlich isotherm:

$$\log q_e = \log K_f + 1/n \log C_e$$

where  $K_f$  and  $1/n$  are constants of adsorption capacity and adsorption intensity, respectively. When Freundlich equation applies,  $\log q_e$  versus  $\log C_e$  will yield a straight line with a slope  $1/n$  and intercept  $K_f$ .

Kinetics of the adsorption experiment was modeled using the pseudo-second order kinetics<sup>19</sup>:

$$t/q_t = 1/k_2q_e^2 + (1/q_e) t$$

and initial sorption rate calculated with the following formula:

$$h = k_2q_e^2$$

where  $h$  is the initial adsorption rate ( $mg\ g^{-1}\ min^{-1}$ ),  $k_2$  is the rate constant ( $g\ mg^{-1}\ min^{-1}$ ),  $q_t$  is the amount of the metal ions on the surface of the adsorbent at any time ( $mg\ g^{-1}$ ) and  $t$  is time (min). If the pseudo-second-order model fits the data,  $t/q_t$  versus  $t$  will have a straight line with a slope  $1/q_e$  and intercept  $1/h$ .

## RESULTS AND DISCUSSION

**Sorption isotherms:** The herbaceous peat adsorbed 96 % of the Cu, Zn and Ni ions and 86 % of Mn ions at  $1 \times 10^{-3}$  M initial solution concentrations and the removal efficiency was similar for Cu (97 %) and lower for Zn (77 %), Mn (68 %) and Ni (75 %) at the highest initial solution concentrations ( $5 \times 10^{-3}$  M). Figs. 1-4 show the plots of the equilibrium solution concentrations *versus* the metal ions sorbed. The adsorption data of the metal ions were fitted to both the Langmuir and Freundlich isotherms (Table-2). Figs. 5 and 6 show Langmuir and Freundlich isotherms for  $\text{Cu}^{2+}$  sorption on to the peat. Langmuir equation better explained the adsorption of the metal ions on the peat compared with the Freundlich equation based on the coefficient of determination ( $R^2$ ) values (Table-2). Several studies have shown that peat-metal ion adsorption is most effectively modeled with the Langmuir isotherm<sup>12,13</sup>. The adsorption capacity (complete monolayer adsorption) of peat was much higher for Cu ( $38.5 \text{ mg g}^{-1}$ ) compared with the other metals ( $24.1\text{-}28.0 \text{ mg g}^{-1}$ ). The adsorption maximum of Zn, Mn and Ni was similar and the affinity of the peat for these metals decreased in the order of Zn, Mn and Ni, respectively (Table-2). Similar order of metal adsorption by peat reported elsewhere<sup>12</sup>. The metal adsorption capacity of peat depends on many factors such as pH, temperature, contact time, peat dose, botanical origin of peat, metal ion and initial metal ion concentration<sup>13,14</sup>. Ho and McKay<sup>20</sup> reported that the copper adsorption capacity of the eutrophic sphagnum moss peats is in the range of  $10\text{-}30 \text{ mg g}^{-1}$  and that of the oligotrophic peats is generally between  $1$  and  $15 \text{ mg g}^{-1}$  based on their literature review. Copper adsorption capacity of peat materials in the similar range was reported elsewhere<sup>14,20-22</sup>.

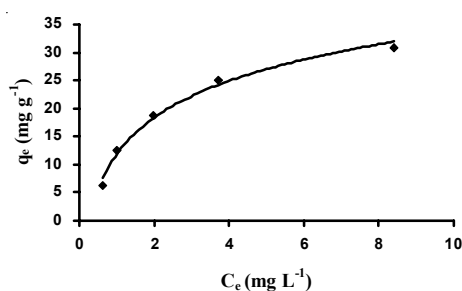
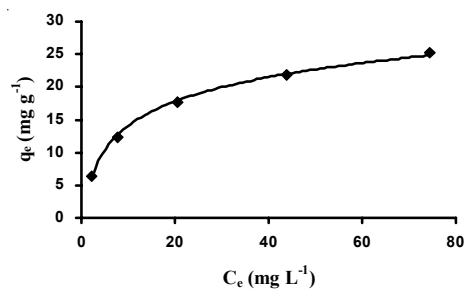
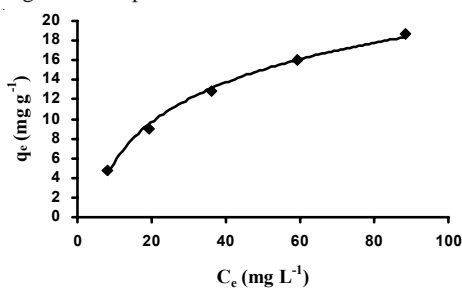
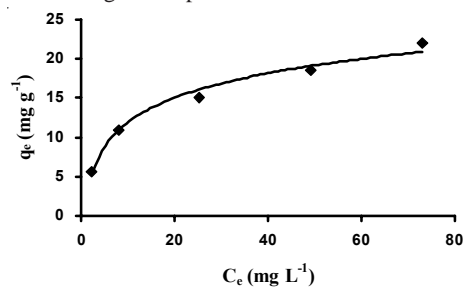
Fig. 1. Sorption isotherm of  $\text{Cu}^{2+}$ Fig. 2. Sorption isotherm of  $\text{Zn}^{2+}$ Fig. 3. Sorption isotherm of  $\text{Mn}^{2+}$ Fig. 4. Sorption isotherm of  $\text{Ni}^{2+}$

TABLE-2  
LANGMUIR AND FREUNDLICH ISOTHERM CONSTANTS  
FOR THE METALS SORBED ON THE PEAT

Element	Langmuir			Freundlich		
	$q_{\max}$	$k$	$R^2$	$K_f$	$1/n$	$R^2$
Cu	38.5	0.49	0.999	13.4	0.42	0.948
Zn	28.0	0.10	0.992	5.1	0.39	0.972
Mn	26.4	0.03	0.999	1.5	0.57	0.977
Ni	24.1	0.09	0.977	4.4	0.38	0.978

\* $q_{\max}$  ( $\text{mg g}^{-1}$ ),  $k$  ( $\text{L mg}^{-1}$ ),  $K_f$  and  $1/n$  are constants.

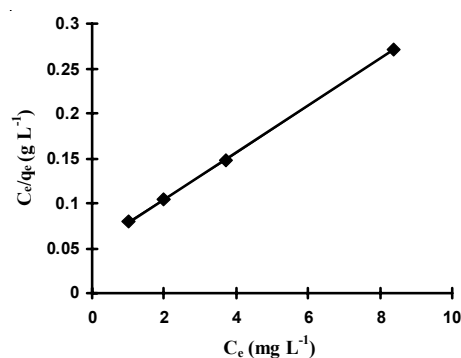


Fig. 5. Langmuir sorption isotherm of  $\text{Cu}^{2+}$  ions

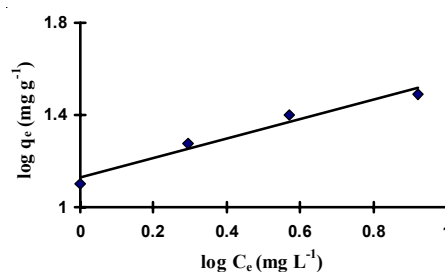


Fig. 6. Freundlich sorption isotherm of  $\text{Cu}^{2+}$  ions

The herbaceous peat material of this study has a neutral pH (6.97) and Ca and Mg are the two important exchangeable cations at this pH<sup>15</sup>. One of the reasons for the relatively high metal adsorption capacity of the Gavur Lake peat can be its high Ca and Mg contents on the exchange sites. Since significant correlation was found between the total exchangeable Ca and Mg contents of peats and their heavy metal adsorption capacity<sup>12</sup>. It was also reported<sup>23</sup> that heavy metals can easily displace  $\text{Ca}^{2+}$  compared to  $\text{H}^+$ . Displacement of Ca and Mg ions with metal ion adsorption was also studied in Cu and Zn experiments (Table-3). A steady increase in equilibrium Ca and Mg ion concentrations were measured as initial metal ion concentrations increased from  $1 \times 10^{-3}$  M to  $5 \times 10^{-3}$  M (Table-3). This finding, therefore, shows that ion exchange is an important mechanism in both Cu and Zn adsorption. The total displaced concentrations of Ca and Mg ions were very similar in both Cu and Zn experiments suggesting that ion exchange was not the only mechanism for the adsorption of Cu, since the peat has much higher adsorption capacity for Cu ( $38.5 \text{ mg g}^{-1}$ ) compared to Zn ( $28.0 \text{ mg g}^{-1}$ ). Chen *et al.*<sup>24</sup> found that the amount of released cations was less than the sorbed Cu ions. They explained this finding with the existence of another mechanism for Cu adsorption in addition to ion-exchange. Metal ion adsorption by peat may take place *via* several mechanisms such as ion-exchange, surface adsorption, chemisorption, complexation and sorption-complexation

TABLE-3  
DISPLACEMENT OF Ca AND Mg IONS WITH INCREASING  
CONCENTRATIONS OF METAL IONS

C <sub>i</sub> (Cu or Zn)	Cu Experiment		Zn Experiment	
	Ca	Mg	Ca	Mg
	mg g <sup>-1</sup>			
1 × 10 <sup>-3</sup> M	4.1	3.9	4.1	4.1
2 × 10 <sup>-3</sup> M	6.1	4.7	5.6	4.5
3 × 10 <sup>-3</sup> M	7.6	5.2	7.0	4.9
4 × 10 <sup>-3</sup> M	9.1	5.4	9.4	5.4
5 × 10 <sup>-3</sup> M	10.3	5.6	10.9	5.4

and it is believed that ion-exchange is the most prevalent mechanism<sup>12</sup>. Bloom and McBride<sup>25</sup> reported that peat binds most divalent cations as outer-sphere complexes or by electrostatic forces with the exception of Cu, which is bound as inner-sphere complexes. The electronic properties of Cu result in formation of strong inner-sphere metal surface complexes and a very strong affinity for soil organic matter<sup>26</sup>.

Freundlich K<sub>f</sub> values, which is a measure of adsorption capacity ranged in the decreasing order of Cu >> Zn > Ni > Mn. The adsorption intensity values determine whether the adsorption is favourable over the entire concentration range (1/n << 1) or favourable at high concentrations and not on low concentrations (1/n > 1)<sup>27</sup>. The adsorption intensity constants were 0.42, 0.39, 0.57 and 0.38 for Cu, Zn, Mn and Ni, respectively, indicating activated adsorption of the metals on the peat. Chen *et al.*<sup>28</sup> reported that the adsorption intensity (1/n) is related to K<sub>f</sub> in the Freundlich equation as part of the power factor and variations in intensity constant will yield exponential change in K<sub>f</sub>. Therefore, higher 1/n value of Mn compared with that of the other metals explains why Freundlich K<sub>f</sub> values of the metals did not rank similar to the Langmuir q<sub>max</sub> values of the metals (Table-2).

**Kinetic study:** Kinetics of the adsorption experiments were modeled using the pseudo-second-order model<sup>19</sup>. The reaction between the metal ions and the peat was very fast and the system reached equilibrium within 0.5 h. The parameters of the pseudo-second-order model was calculated by regressing t/q<sub>t</sub> versus t for the initial metal concentrations of 2 × 10<sup>-3</sup> M and 4 × 10<sup>-3</sup> M (Table-4). The kinetic data

TABLE-4  
PSEUDO-SECOND-ORDER MODEL PARAMETERS OF THE METALS AT  
2 × 10<sup>-3</sup> M AND 4 × 10<sup>-3</sup> M INITIAL SOLUTION CONCENTRATIONS

Element	2 × 10 <sup>-3</sup> M				4 × 10 <sup>-3</sup> M			
	q <sub>e</sub> *	h	k <sub>2</sub>	R <sup>2</sup>	q <sub>e</sub>	h	k <sub>2</sub>	R <sup>2</sup>
Cu	12.6	169.4	1.07	0.999	24.9	145.6	0.23	0.999
Zn	12.2	54.6	0.37	0.999	21.9	149.3	0.31	0.999
Mn	9.2	60.1	0.71	0.999	16.9	47.2	0.17	0.999
Ni	10.8	51.9	0.44	0.999	19.3	79.2	0.21	0.999

\*q<sub>e</sub> (mg g<sup>-1</sup>), h (mg g<sup>-1</sup> min<sup>-1</sup>), k<sub>2</sub> (g mg<sup>-1</sup> min<sup>-1</sup>).

showed a good fit to the pseudo-second-order model (Fig. 7). Equilibrium metal adsorption ( $q_e$ ) of the peat at  $2 \times 10^{-3}$  M and  $4 \times 10^{-3}$  M initial solution concentrations were in the following order  $\text{Cu} > \text{Zn} > \text{Ni} > \text{Mn}$ . The affinity of the metals for the peat at these concentrations was similar to the rank of the Freundlich  $K_f$  values. Initial adsorption rate ( $h$ ) of Cu ions ( $169.4 \text{ mg g}^{-1} \text{ min}^{-1}$ ) was much higher than that of the other metals at  $2 \times 10^{-3}$  M initial solution concentrations. The adsorption rate constant ( $k_2$ ) also followed the same trend. The initial adsorption rates of Cu and Mn decreased and that of Zn and Ni increased as initial metal ion concentration increased from  $2 \times 10^{-3}$  M to  $4 \times 10^{-3}$  M (Table-4). The adsorption rate constants of the studied metals, however, decreased with an increase in initial metal ion concentrations. Negative relationship between the rate constant and initial metal ion concentration was also reported elsewhere<sup>29</sup>.

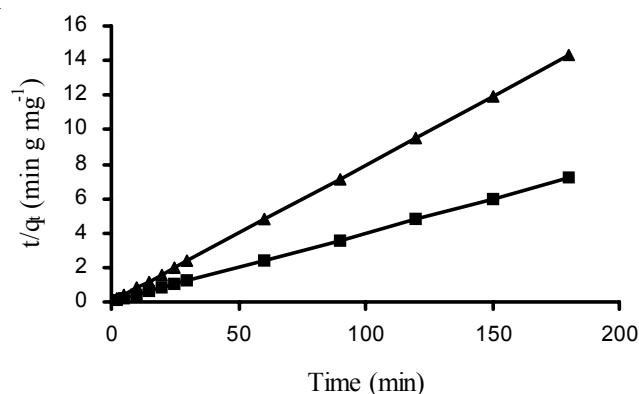


Fig. 7. Pseudo second-order kinetics of  $\text{Cu}^{2+}$  at  $2 \times 10^{-3}$  M (▲) and  $4 \times 10^{-3}$  M (■) initial solution concentrations

**Effect of solution pH:** Solution pH is an important factor affecting the capacity of peat to hold cations and optimum pH for adsorption<sup>12</sup> is between 3.5 and 6.5. The effect of solution pH on the metal adsorption was studied for solution pH values 3, 4 and 5 at  $2 \times 10^{-3}$  M metal ion concentrations. The equilibrium time was 3 h at  $21 \pm 1$  °C. Fig. 8 shows that Cu adsorption was not affected in this pH range but the adsorption of Zn, Mn and Ni was lower at pH 3 compared with pH 4 and 5. Similar adsorption of the metals at pH 4 and 5 was probably due to buffering effects of the peat and at pH 3 high concentrations of  $\text{H}^+$  ions lowered metal adsorption by ion exchange. Ringqvist and Öborn<sup>14</sup> reported that the solution pH has minor effect on Cu adsorption on peat but it was one of the main factors affecting Zn adsorption.

## Conclusion

(1) The adsorption of the metal ions on to the peat fitted both Langmuir and Freundlich models and the Langmuir model better explained the adsorption. The adsorption capacity of the peat followed the order  $\text{Cu} > \text{Zn} > \text{Mn} > \text{Ni}$ . (2) The peat

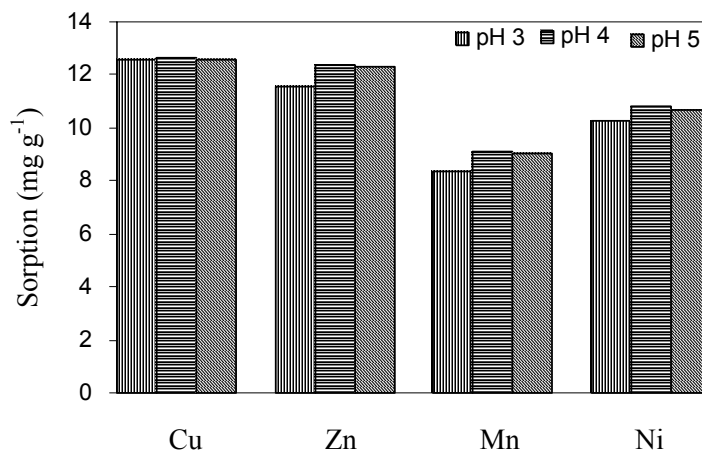


Fig. 8. Effect of initial pH on the sorption of the metal ions for  $2 \times 10^{-3}$  M initial solution concentrations

removed 86-96 % of the metal ions at the lowest initial concentrations and between 68-97 % of the metal ions at the highest initial solution concentration and Cu was the most efficiently removed metal ion in both low and high initial solutions (96 and 97 %). (3) The kinetic study revealed that the adsorption followed the pseudo-second-order model and the interaction between the metal ions and the peat was very fast and equilibrium was reached within 0.5 h. (4) Cu adsorption was not affected in the pH range between 3 and 5 but the adsorption of Zn, Mn and Ni was lower at pH 3 compared with pH 4 and 5.

## REFERENCES

1. R.B. Martin, *Metal Ions in Biological Systems, Concepts on Metal Ion Toxicity*, Marcel Dekker, New York and Basel, p. 21 (1986).
2. A.K. Meena, G.K. Mishra, P.K. Rai, C. Rajagopal and P.N. Nagar, *J. Hazard. Mater.*, **122**, 161 (2005).
3. M. Sprynskyy, B. Buszewski, A.P. Terzyk and J. Namiesnik, *J. Colloid Interface Sci.*, **304**, 21 (2006).
4. S.E. Bailey, T.J. Olin, R.M. Brica and D.D. Adrin, *Water Res.*, **33**, 2469 (1999).
5. T. Mathialagan and T. Viraraghavan, *J. Hazard. Mater.*, **94**, 291 (2002).
6. T. Mathialagan and T. Viraraghavan, *Sep. Sci. Technol.*, **338**, 57 (2003).
7. O. Yavuz, Y. Altunkaynak and F. Guzel, *Water Res.*, **37**, 948 (2003).
8. Y.S. Ho, *Water Res.*, **37**, 2323 (2003).
9. Y.S. Ho and A.E. Ofomaja, *J. Hazard. Mater.*, **120**, 157 (2005).
10. D. Wankasi, M.J. Horsfall and A.I. Spiff, *Electronic J. Biotechnol.*, **9**, 587 (2006).
11. I.J. Alinnor, *Fuel*, **86**, 853 (2007).
12. P.A. Brown, S.A. Gill and S.J. Allen, *Water Res.*, **34**, 3907 (2000).
13. Y.S. Ho and G. McKay, *Water Res.*, **34**, 735 (2000).
14. L. Ringqvist and I. Öborn, *Water Res.*, **36**, 2233 (2002).
15. H. Dikici and C.H. Yilmaz, *J. Environ. Qual.*, **35**, 866 (2006).
16. D.W. Nelson and L.E. Sommers, *Methods of Soil Analysis: Chemical Methods*, Part 3, Madison, WI, p. 961 (1996).



17. G.W. Thomas, *Methods of Soil Analysis: Chemical Methods, Part 3*, Madison, WI, p. 475 (1996).
18. R.H. Loeppert and D.L. Suarez, *Methods of Soil Analysis: Chemical Methods, Part 3*, Madison, WI, p. 437 (1996).
19. Y.S. Ho, *J. Hazard. Mater.*, **136**, 681 (2006).
20. Y.S. Ho and G. McKay, *Water, Air Soil Pollut.*, **158**, 77 (2004).
21. F. Qin, B. Wen, X.Q. Shan, Y.N. Xie, T. Liu, S.Z. Zhang and S.U. Khan, *Environ. Pollut.*, **144**, 669 (2006).
22. R. Gündogan, B. Acemioglu and M.H. Alma, *J. Colloid Interface Sci.*, **269**, 303 (2004).
23. A. Wolf, K. Bunzl, F. Dietl and W.F. Schmidt, *Chemosphere*, **6**, 207 (1977).
24. X.H. Chen, T. Gosset and D.R. Thevenot, *Water Res.*, **24**, 1463 (1990).
25. P.R. Bloom and M.B. McBride, *J. Soil Sci. Soc. Am.*, **43**, 678 (1979).
26. N.T. Basta, J.A. Ryan and R.L. Chaney, *J. Environ. Qual.*, **34**, 49 (2005).
27. Y.S. Al-Degs, M.I. El-Barghouthi, A.A. Issa, M.A. Khraisheh and G.M. Walker, *Water Res.*, **40**, 2645 (2006).
28. Z. Chen, B. Xing and W.B. McGill, *J. Environ. Qual.*, **28**, 1422 (1999).
29. Y.S. Ho, G. McKay, D.A.J. Wase and C.F. Forster, *Adsorp. Sci. Tech.*, **18**, 639 (2000).

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